

- Write a MATLAB program to evaluate $I = \int_a^b f(x) dx$ using the trapezoidal rule with n subdivisions, calling the result I_n . Use the program to calculate the following integrals with $n = 2, 4, 8, 16, \dots, 512$.

$$(a) \int_0^1 e^{-x^2} dx \quad (b) \int_0^1 x^{3/2} dx$$

Try to arrange your work so that you never compute the value of the integrand at any point more than once. Analyze empirically the rate of convergence of I_n to I by calculating the ratios

$$R_n = \frac{I_{2n} - I_n}{I_{4n} - I_{2n}} \text{ and } p_n = \frac{\log(R_n)}{\log(2)}$$

- Repeat problem 1 using Simpson's rule.
- Apply the corrected trapezoidal rule to the integrals in problem 1. Compare the results with those of problem 2 for Simpson's rule.
- Use Gauss-Legendre integration with $n = 2, 4, 8$ nodes to the integrals of problem 1. Compare the results with those for the trapezoidal and Simpson methods.
- Use the MATLAB function QUADL to find approximate values of the integrals 1(a) and 1(b).
- Ex. 5.1, p.183, *Shampine, Allen & Preuss*.
- The 11 point Newton-Cotes integration rule on $[0, 1]$ is

$$\int_0^1 f(x) dx \approx \sum_{i=0}^{10} w_i f\left(\frac{i}{10}\right)$$

with the w_i determined by requiring that the rule be exact for $f(x) = 1, x, x^2, \dots, x^{10}$.

- Use MATLAB to find the weights w_i .
 - Apply the rule to the integrals in 1(a) and 1(b). Note the errors.
- We wish to estimate the value of

$$I = \int_0^{\infty} \exp(-x) \cos^2 x dx = .6$$

- Truncate the integral and use QUADL on the finite part.
- Try the transformation $x = -\ln t$ on this integral and use QUADL on the new integral.
- Use the 2, 4 and 8 point Gauss-Laguerre rules to estimate the integral. compare your results with parts (a) and (b) above.

9. In a standard shell and heat exchanger hot vapor condenses on the tube, maintaining a constant temperature T_s . If the input is at temperature T_1 and the output must be at temperature T_2 , then the length of tube required is given by

$$L = \frac{m}{\pi D} \int_{T_1}^{T_2} \frac{c_\rho dT}{h(T_s - T)}.$$

(All quantities must be in consistent units.) Here T is the temperature in $^{\circ}\text{F}$.

$T_1 = 0^{\circ}\text{F}$ is the inlet temperature.

$T_2 = 180^{\circ}\text{F}$ is the desired outlet temperature.

$T_s = 250^{\circ}\text{F}$ is the condensate temperature.

m is the fluid flow rate = 45,000 lb/hr.

D is the diameter of the tube = 1.032 in.

c_ρ is the specific heat of the fluid = $(0.53 + 0.00065T)$ BTU/(lb $^{\circ}\text{F}$).

h is the local heat transfer coefficient = $\frac{0.023k}{D} \left(\frac{4m}{\pi D\mu}\right)^{0.8} \left(\frac{\mu c_\rho}{k}\right)^{0.4}$.

k is the thermal conductivity of the fluid = 0.153 BTU/(hr ft $^{\circ}\text{F}$).

μ is the viscosity of the fluid and has units lb/(ft hr). μ varies with temperature so that

T	0	50	100	150	200
μ	242	82.1	30.5	12.6	5.57

Use spline interpolation to define μ for other values of T and calculate the required length of the heat exchanger.

You will need to use the MATLAB functions SPLINE and QUADL. The answer is about 158.7 ft.